



Specifics of Forced-Convective Heat Transfer in Supercritical Carbon Dioxide

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Summary

The appropriate description of heat-transfer to coolants at supercritical state is one of the main challenges in development of supercritical-fluids applications for the Generation-IV reactors. In this paper the basis for comparison of relatively recent experimental data on supercritical carbon dioxide (CO₂) obtained at facilities of the Korea Atomic Energy Research Institute (KAERI) and Chalk River Laboratories (CRL) of Atomic Energy of Canada Limited (AECL) is discussed, and a preliminary heat-transfer correlation for joint CRL and KAERI datasets is presented.

1. Introduction

The majority of experiments with forced convective flow of fluid at SuperCritical (SC) state where done with water. Starting from early experiments in the late 50's and early 70's [1-6], the general behavior of SuperCritical Water (SCW) was described. Researchers have noticed that at a certain combination of inlet parameters, the wall temperature along the heated part of the tube for SCW flow would experience a sharp increase. Such generic behavior was called a Deteriorated Heat Transfer (DHT). It was also noticed that DHT at SC conditions caused much smoother wall temperature distribution and lesser temperature jumps compared to the case of DHT caused by reaching Critical Heat Flux (CHF) at subcritical conditions. Although researchers spotted similar behavior, the actual data on heat transfer to SCW showed considerable variations [7-8], and, therefore, criteria for the onset of DHT proposed by various authors differ and often contradict each other. In addition to this, numerous semi-empirical models proposed to describe the experimental data since the mid 60's turned out to satisfactorily describe just the data they were designed for. In the end, finding these data is generally a challenging task for the following reasons:

- 1) Generally, these data are commercial or proprietary.
- 2) Many datasets, especially, those obtained before 1965, were lost. In some cases, investigators who knew the location of the data died or retired; in some cases, the data were never properly archived; in other cases, laboratories, where the data were obtained were closed (e.g., UKAEA) [9]. Groeneveld *et al.* estimated that only a half of the originally reported data on heat transfer to water at SC conditions is available [9].

- 3) The bulk of available data are in graphical form. Accuracy of digitized data depends both on the quality of the original graphs and also on the quality of the digitizing software. Moreover, experimentalists would be able to publish just small portions of their data due to the limitations of publications.

Therefore, due to the importance of resolving the problem of accurate prediction of heat transfer to SCW, the International Atomic Energy Agency (IAEA) established a coordinated research project "Heat Transfer Behavior and Thermal-Hydraulics Code Testing for Super-Critical Water-cooled Reactors". The first step of this project is to "establish a base of accurate data for heat transfer, pressure drop, blowdown, natural circulation, and stability for conditions relevant to super-critical fluids [10].

Since the critical parameters of water are very high (22.064 MPa and 374.1°C), performing forced-convection heat-transfer experiments in SCW is a complex and expensive task. Therefore, it is reasonable to study general properties of SC fluids by running experiments with modeling fluids (sometimes, the term 'surrogate fluids' is used instead). CO₂ and R-134a are the two most widely used modeling fluids. Under certain conditions, the results can be later interpreted and scaled to SCW conditions (for a discussion on proper scaling methodology, see References [11-12]). In comparison, critical parameters of CO₂ (7.38 MPa and 31.08°C) are significantly lower than those of SCW (see Figure 1).

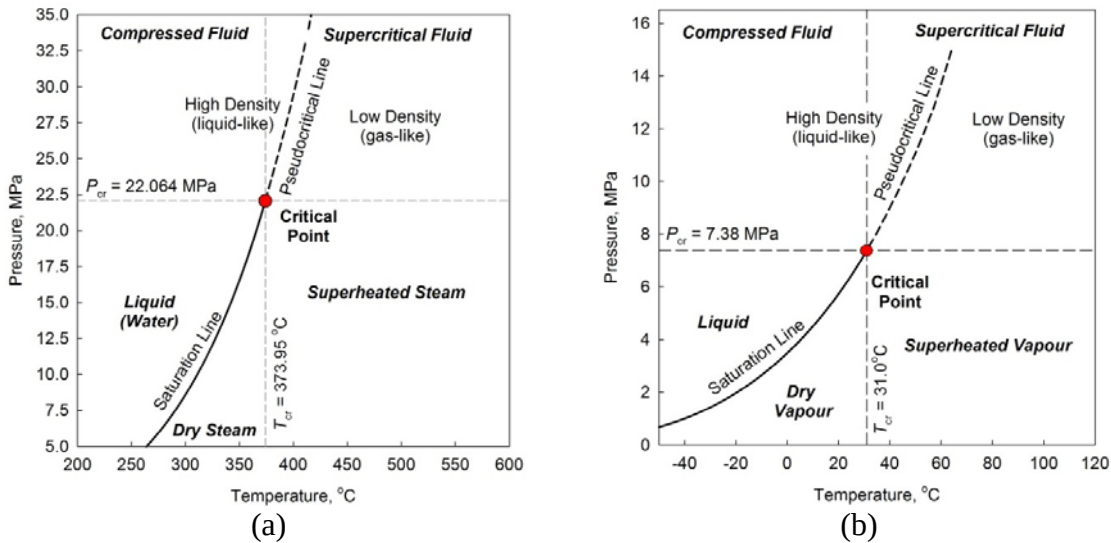


Figure 1. Pressure-temperature diagram for water (a) and CO₂ (b) (data were calculated using NIST Refprop v9.0)

The development of sophisticated theoretical models is very important for improving the understanding of physical processes behind the forced-convective heat-transfer and its deterioration in the near-critical region. However, not all turbulent models implemented in Computational Fluid Dynamics (CFD) codes are applicable to heat transfer at supercritical pressures. Numerous recent worldwide CFD studies showed that models based on the Reynolds

number Averaged Navier-Stokes (RANS) equations are able to capture temperature trends at normal conditions and predict the onset of deterioration; however, these models fail to capture deteriorated heat transfer numerically [13-17]. It should be noted that in most of these works, CFD results were validated based on old data presented in [5-6], [18]. Only one study was validated against more recent data [resented in [19]. Therefore, there is still a great reliance on 1D heat-transfer correlations for fast preliminary calculations.

The majority of empirical correlations were proposed in the 1960s – 1970s, when experimental techniques were not at as advanced level as they are today. Also, thermophysical properties of fluids have been updated since that time (for example, a peak in thermal conductivity of water in critical and pseudocritical points within a range of pressures from 22.1 to 25 MPa was not officially recognized until the 1990s) [14], [20]. Although, there were numbers of more recent correlations developed for water [21-24], there were only two recent correlations proposed for CO₂ (see [25-26]) based on the data obtained by Dr. Pioro at Chalk River Laboratories (CRL) [7]. Unfortunately, previous analysis of the latter two correlations (Saltanov *et al.*, 2013) showed that they fail to predict SC CO₂ data obtained in different experiments. Therefore, they should be revised, and the reason for their failure must be established. Also, data on heat transfer to SCW used at SC fossil-fired plants cannot be used directly, because typical hydraulic diameters are around 18 mm, while in SuperCritical Water-cooled Reactors (SCWRs) those will be between 4 – 9 mm. This significantly affects the development and distribution of velocity and thermal fields across the heated channel.

2. Basis for Comparison of the Joint Datasets

The KAERI and AECL datasets were compared based on the similarity of heat flux at the inlet to test-section (see Figures 2–3).

The following are the major conclusions of this comparison:

- The results are consistent for the same geometry and slight variation of input parameters;
- There is a clear similarity in the pattern of the data between different geometries in the cases of close values of heat and mass fluxes. Similarity based on $\frac{T_b}{T_{pc}}$ may be one of

the uniting parameters for the experimental data.

The major problem of this comparison is the lost information on the location. The authors of this paper expect that behavior could be better generalized based on the non-dimensional “coordinate” which is introduced here as follows:

$$X = \frac{h_b - h_{pc}}{q / G} \quad (1)$$

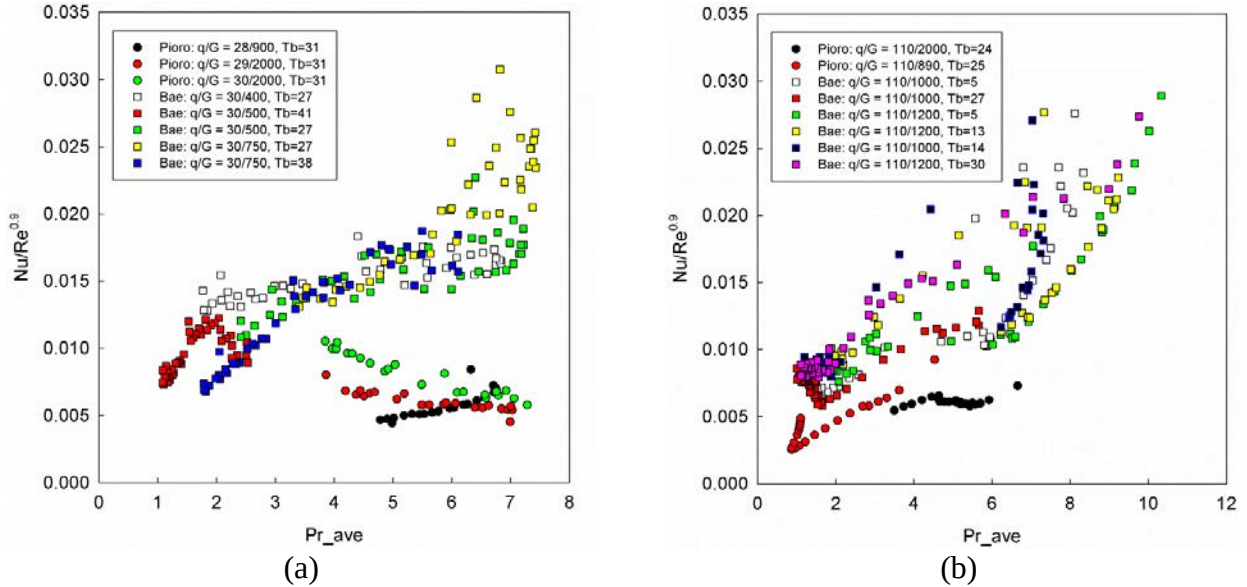


Figure 2. Comparison of KAERI and AECL data based on similarity of heat flux at the inlet to the test-section (a – $P=8.85$ MPa, $q=30$ kW/m², $d=4.4$ mm (KAERI), $d = 8.1$ mm (AECL); b – $P=7.75$ MPa, $q=110$ kW/m², $d=4.4$ mm (KAERI), $d = 8.1$ mm (AECL));

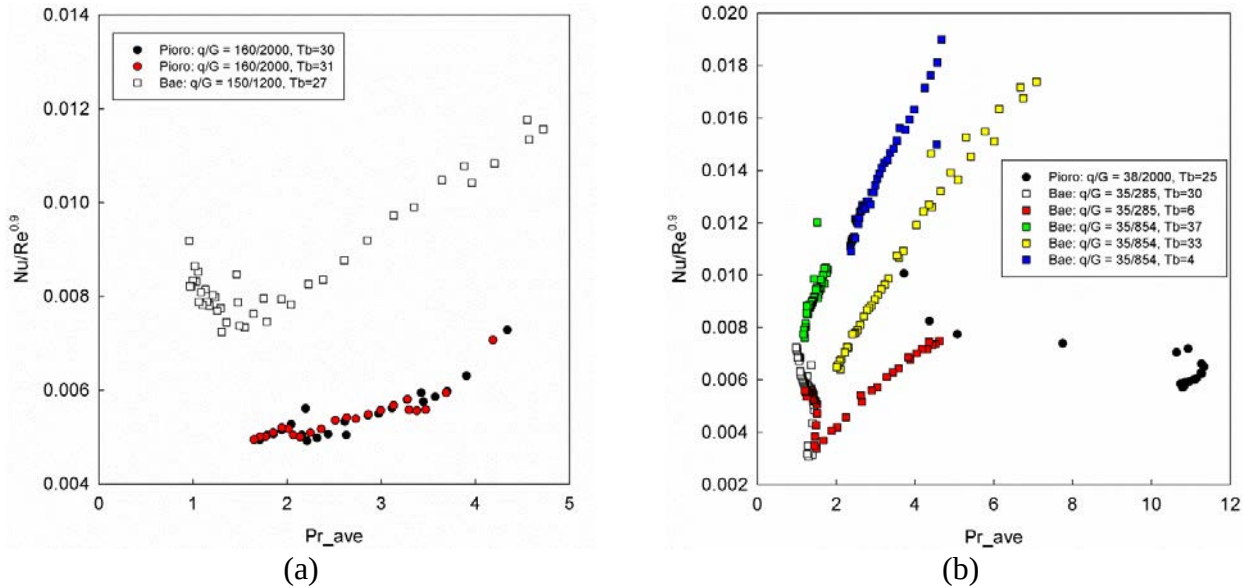


Figure 3. Comparison of KAERI and AECL data based on similarity of heat flux at the inlet to the test-section (a – $P=8.85$ MPa, $q=150$ kW/m², $d=4.4$ mm (KAERI), $d = 8.1$ mm (AECL); b – $P=7.75$ MPa, $q=35-38$ kW/m², $d=6.32$ mm (KAERI), $d = 8.1$ mm (AECL));

3. A Preliminary Heat-Transfer Correlation for Joint CRL and KAERI datasets.

Following the methodology discussed in Reference [27], the authors developed the following preliminary correlation for joint CRL and KAERI data:

$$\text{Nu}_b = 0.0364 \text{Re}_b^{0.778} \overline{\text{Pr}}_b^{-0.413} \left(\frac{\rho_w}{\rho_b} \right)^{0.656} \quad (2)$$

(All symbols are defined in Section 5). DHT points were removed based on a visual inspection, and points affected by buoyancy were removed as well.

The RMS for this correlation is 23% for HTC and 4% for T_w . The range of applicability of correlation Eq. (2) is shown in Table 1. Due to the limitations on the size of the extended abstract the authors cannot present or discuss more of their work on the subject.

Table 1. Range of applicability of Eq. (2).

P , MPa	G , kg/m ² s	q , kW/m ²	T_b , °C	D , mm
7.57–8.91	199–3048	9.9–616	5–161	4.4–9.0

4. Conclusions

A basis for comparison of the KAERI and AECL datasets was discussed. The discussion prompted an idea to generalize data based on a new non-dimensional “coordinate”, which was introduced in the paper. Based on a standard methodology, a preliminary correlation for joint CRL and KAERI data was presented. Although RMS error is quite high (23%), the correlation is considered as a success, because it is valid for a wide range of experimental parameters and hydraulic diameters.



5. Nomenclature

Symbols

d, D	hydraulic diameter, mm
G	mass flux, kg/m ² ·s
h	specific enthalpy, J/kg
k	thermal conductivity, W/m·K
P	pressure, Pa
q	heat flux, W/m ²
T	temperature, K

Greek Letters

μ	dynamic viscosity, Pa·s
ρ	density, kg/m ³

Dimensionless Numbers

Nu	Nusselt number $\left(\frac{HTC \cdot D}{k} \right)$
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Pr_{ave}, Pr	Average Prandtl number $\left(\frac{h_w - h_b}{T_w - T_b} \cdot \frac{\mu}{k} \right)$
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Re

$$\text{Reynolds number} \left(\frac{G \cdot D}{\mu} \right)$$

Subscripts

ave	average
b	bulk-fluid
pc	pseudocritical
w	wall

Acronyms

CFD	Computational Fluid Dynamics
CHF	Critical Heat Flux
CRL	Chalk River Laboratories
DHT	Deteriorated Heat Transfer
HTC	Heat Transfer Coefficient
IAEA	International Atomic Energy Agency
KAERI	The Korea Atomic Energy Research Institute
RANS	Reynolds number Averaged Navier-Stokes equations
RMS	Root Mean Square
SC	SuperCritical
SCW	SuperCritical Water
SCWR	SuperCritical Water-cooled Reactor
UKAEA	United Kingdom Atomic Energy Authority

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