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# TOPFLOW-PTS EXPERIMENTS. PRE-TEST CALCULATIONS WITH NEPTUNE\_CFD CODE

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#### **Abstract**

Hypothetical Small Break Loss Of Cool ant Acc ident is identified as one of the most severe transients leading to a potential huge Pressurized Thermal Shock on the Reactor Pressure Vessel (RPV). This may result in two-phase flow configurations in the cold legs, according to the operating conditions, and to reliably assess the RPV wall integrity, advanced two-phase flow simulations are required. Related needs in development and/or validation of these advanced models are important, and the on-going TOPFLOW-PTS experimental program was designed to provide a well documented data base to meet these needs. This paper focuses on pre-test NEPTUNE\_CFD simulations of TOPFLOW—PTS experiments; these simulations were performed to (i) help in the definition of the test matrix and test procedure, and (ii) check the presence of the different key physical phenomena at the mock-up scale.

#### 1. Introduction

In the frame of l ifetime extension of Pr essurized Water Reactors (PWR), Pressurized Thermal Shock (PTS) along the Reactor Pressure Vessel (RPV) wall is one of the most crucial concerns with respect to its i ntegrity. To assess the R PV integrity and evaluate the lifetime of French (PWR type) N uclear Pow er Plants (N PP), ED F and A REVA have developed a three-step methodology including (Figure 1) (i) syst em-code calculations to define the transients related scenarios and associated boundary conditions needed for the further step, (ii) coupled "CFD-Heat conduction" simulations to determine the thermal loads within the RPV wall s, and (iii) a subsequent mechanical analysis.

Related an alyses have shown that on e of the most severe loading conditions is given by the Small Break Loss Of Cool ant Accidents (SBLOCA). During this type of hypothetical LOCA, cold Emergency Core Cooling (ECC) water is injected into the cold leg and partially mixes with the hot primary fluid flow down to the downcomer, possibly resulting in a large PTS on mechanical structures, first of all on the RPV wall. Depending on the accident transient scenario - leak size and location for example - and on the operating conditions of the considered NPP, a single-phase or two-phase flow configuration can exist in the cold legs.

Actually, the current RPV wall int egrity dem onstration has to consi der accident transient s resulting in two-phase flow configurations, and further requires dedicated two-phase flow CFD simulations. Direct Contact Condensation (DCC), mixing and flow-to-wall heat transfer are of prime importance in this situation. These phenomena are strongly influenced by the structure of the water-steam interface and by turbulence, and related interfacial transfers (mass, momentum – including turbulence – and energy) have then to be reliably represented by the CFD simulations. It is the us necessary to develop and/or validate specific models, which have to accurately represent (i) the highly turbulent bubbly flow in the ECC impinging jet area, and (ii) the thermal stratification of the water-steam flow along the cold leg downstream from the ECC nozzle, as well as (iii) the single-phase flow in the down comer, including the flow-to-wall heat transfer along the cold leg and RPV wall.

After a fir st R& D work st age be ing per formed for se veral ye ars, a significant extensive engineering work devoted to the RPV stru ctural integrity re-assessment for the French 900 and 1300 MW e PW Rs is in progress at EDF and it s French partners ([1] to [3]). Numerous developments have been implemented or are in progress to make sure the CFD methodology reliably represents the flow during a PTS even t. The on-going TOPFLOW-PTS experimental program [4] was designed in this frame. It aims at providing a well documented database to further (i) complement the validation of the whole CFD modelling in PTS t wo-phase configurations, (ii) improve the understanding of the involved key physical T/H phenomena, and (iii) as far as possible enable the validation and/or development of the related models and closure laws.

After a general overview of TOPFLOW-PTS experimental program, this paper is devoted to pretest CFD simulations of TOPFLOW-PTS experiments including both air/water and steam/water configurations. Such pre-test simulations were carried out with NEPTUNE\_CFD code to help in the definition of the test matrix, and possibly of the test procedure, checking to what extent the different key phy sical phenom ena of interest are pre-sent a nd can be "c aught" by the implemented instrumentation.

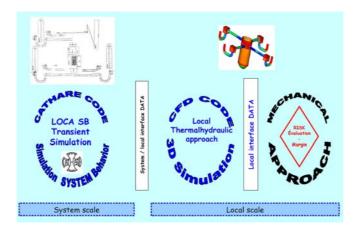


Figure 1 Chaining computation methodology

# 2. TOPFLOW-PTS experimental setup

#### 2.1 General

The TOPFLOW-PTS was designed in 2005 after the identification (within the frame of French joint NEPTUNE Project [5]) of pending validation data needs for the CFD m odeling of PTS Thermal Hydraulics (T/H) concerns in the two-phase configuration. Actually, these validation data needs were related to the local modelling of the afore-mentioned key physical phenomena and a priori required separate-effect experiments; however, considering:

- (i) these ph enomena are m ostly very tightly coup led and DCC is important in the who le process, and
- (ii) the need for a well instrumented experiment of the combined phenomena over the whole domain of interest for validation and demonstration purposes with respect to the actual industrial application,

it was decided to set up an integral-type experimentation—TOPFLOW-PTS - heavily instrumented with state-of-the-art local measurement techniques.

The TOPFLOW-PTS experimental program is based on (i) the 900 MWe CPY NPPs operated in France, and (ii) a SB LOCA scenario. It is jo intly operated and/ or financially sup ported by AREVA (France), Commissariat à l'E nergie A tomique (CEA, France), Electric ité de France (EDF, France), S wiss Federal Institute of Technology of Zürich (ETHZ, Swi tzerland), Helmholtz-Zentrum Dresden-Ro ssendorf (HZDR - formerly FZ D, Ger many), In stitut de Radioprotection et de Sûreté Nucléaire (IRSN, France) and Paul Scherr er Inst itut (PSI, Switzerland).

#### 2.2 Main features

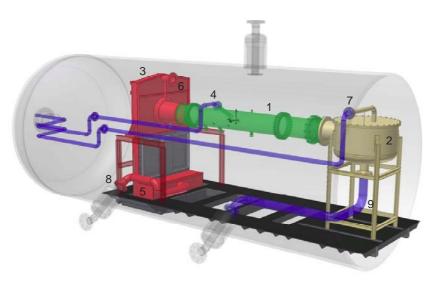
The PTS test section (Figure 2) models the cold leg with the ECC injection line, a primary pump and a part of the downcomer of the reference CPY plant in a 1:2.5 geometrical scale, with some simplifications i.e. (i) a straight cold leg, (ii) a flat downcomer representing a 90° segment of the reference plant, and (iii) a pump simulator – actually a vessel 1 ocated upstream from the ECC injection nozzle. This pump simulator can be supplied with water at its top and water-drained at its lowest point, so that steady-state tests can be achieved with an a ctual thermal stratification along the cold leg.

This test section is connected to the HZDR TO PFLOW facility and installed in the so-called *diving tank*, which allows test performance at up to 5 MPa and 265 °C conditions, at pressure equilibrium with the tank nitrogen atmosphere, along with a thin-walled test section design for implementation of infra-red thermography. Its is instrumented with:

(i) 196 thermocouples distributed within the cold leg and downcomer flow, as well as in a so-called *Heat Flux Probe* – HFP (it is actually a thick steel bar integrated in the downcomer front wall);

- wire mesh sensors along the cold leg (i mpinging jet and stratified flow areas), as well as (ii) "TC-void probes" (impinging jet area), to provide information on the bubbly gas phase, water level and surface wave structure, and possibly liquid phase velocity;
- a high-speed camera for the observation of the impinging jet area from the back wall of the downcomer, and an inf ra-red camera for a ther mography of the cold leg wall and of the downcomer front wall.

The test program includes (on-going) performance of transient and/or steady-state tests, with and without mass transfer (i.e. with water ECC injection in a steam or a nit rogen en vironment, respectively), u p t o a 5 MPa pressure. Test parameters ar e v aried ar ound the scaled-down reference condition set.



- 1 cold leg 2 pump simulator
- downcomer
- 4 ECC injection pipe
- 5 outlet water box
- steam supply pipe
- 7 pump simulator feed water pipe
- 8 downcomer drainage pipe
- pump simulator drainage pipe

Figure 2 Test section scheme

#### **3. NEPTUNE CFD computer code**

#### 3.1 General features

NEPTUNE CFD is the multi-phase CFD solver of the NEPTUNE software platform [5], jointly developed by CEA and EDF with a complementary support of AREVA and IRSN. This platform is dedicated to advanced two-phase flow thermal-hydraulics, allowing multi-scale and multidisciplinary cal culations m eeting the i ndustrial needs (am ong which PTS i nt wo-phase configuration). NEPTUNE CFD has also be een chosen as a basis for the development of CFD tools in the international shared so ftware platform for nuclear therm al-hydraulics developed in the European fram ework, i.e. former NURESIM [6] project and furth er today NURISP project (see [7] presented in CFD4NRS conference).

The basic model of N EPTUNE\_CFD is the classical six-equation two-fluid model (mass, momentum and energy for both liquid and gas, with the same pressure for the two phases), coupled to a k-ε model for the continuous phases, and (optionally) a transport equation for the interfacial area concentration.

From a numerical point of view, the spatial discretization is based on a co-located finite volume approach that ac cepts m eshes with any type of cell (tetrahedral, hex ahedral, prismatic, pyramidal, polyhedral...) and any type of grid structure (unstructured, block structured, hybrid, conforming or with hanging nodes...), while the solver algorithm is an original method dedicated to multi-phase systems [8].

# 3.2 PTS-related model developments in NEPTUNE\_CFD

In the frame of NEPTUNE\_CFD development for PTS-related application, a special attention is paid to the modelling of (i) the detection of the position of the gas-liquid interface in the stratified flow area, (ii) the turbulence, especially close to the free surface, and (iii) the heat and mass transfer close to the free surface at the gas-liquid interface and in the impinging jet area.

#### 4. **NEPTUNE\_CFD** pre-test simulations

# 4.1 Objectives

Initially, the NEPTUNE\_CFD pre-test simulations aimed at refining the test section design and helping the definition of the test m atrix and experimental procedure; in this frame, the related result analyses checked to what extend the key physical phenomena of the industrial scenario are present at the mock-up scale and with the foreseen operating conditions.

#### 4.2 Geometry and grid

Figure 3 illustrates the CAD model of the TOPFLOW-PTS test section.

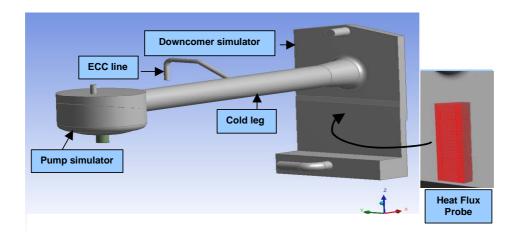


Figure 3 CFD model of the TOPFLOW-PTS test section

The fluid domain is represented with 431 330 hexagonal cells whereas the HFP solid mesh is represented with 58320 tetrahedral cells.

# 4.3 Initial and boundary conditions

The allowed boundary conditions in terms of mass flow rate and temperature are represented in Figure 4. There are:

- (i) 3 fluid inlets: the cold water inlet at the ECC injection nozzle, the "hot" feedwater inlet at the top of the pump simulator and the gas inlet at the top of the downcomer. Whereas the temperature and mass flow rate are exp licitly imposed for the ECC injection and pump feed water, they step-by-step result from the simulation for the gas inlet at the top of the downcomer;
- (ii) 3 fluid outlets: the water outlet at the bottom of the downcomer, the gas outlet at the top of the downcomer and the water outlet at the bottom of the pump simulator (to drain the flow coming from the cold leg). Note only the latter outlet flowrate is prescribed as an explicit boundary condition; the two former ones are based on simulation results at each time step to respectively maintain a constant water level in the cold leg and a constant pressure in the test section atmosphere.

Finally, at the beginning of the calculation, the cold leg is (otherwise differently specified) filled in water and the water level is decreased (with the ECC injection in operation) down to the cold leg mid-plane ("50 % level") during the first step of the simulation; during the subsequent second step, it is maintained at a 50 % value. Sect ion 6.2 devoted to the gas-li quid flow separ ation occurrence in the ECC line will point out the importance of this procedure.

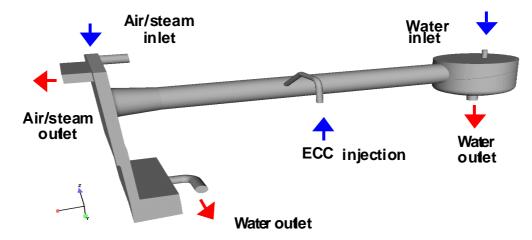


Figure 4 Boundary conditions allowed for the TOPFLOW-PTS simulations

# 4.4 Physical properties, physical and numerical models

For wa ter a nd st eam, t he CATHARE water/steam properties (implemented in the NEPTUNE\_CFD code) were u sed to calculate density, thermal diffusivity, specific heat and dynamic viscosity over a large range of temperature and pressure. For air, the needed properties were assumed as constants.

For the solid domain, specific heat and thermal conductivity were dependent on temperature, but not density.

The Large Interface Model [9] was used for the modeling of the free surface. Heat transfers between phases were modeled only for the steam/water cases. Simulations were performed with a thermal coupling between the fluid and the solid domains, with a time step computed in order to respect a CFL lower than 1.

#### 5 Results and analysis

#### 5.1 Pre-test simulation series performed and associated objectives

Two pre-test simulation series were performed. They were respectively focused on:

- (i) the flow pattern in the ECC injection line, with the possible existence of a gas-liquid flow separation. Parametric simulations in air/water and steam/water configurations were thus carried out in turn, to check the rel ated ECC flowrate threshold, the existence of any possible hysteresis phenomenon as well as of any test conditions and procedure impact;
- (ii) the presence of T/H k ey phenomena in the foreseen experimental tests; one air/water and one steam/water configurations (with constant boundary conditions) were considered. The qualitative and quantitative analyses were mainly related to the therm all stratification and associated gradient amplitude in the cold leg and downcomer, over the transient operation till the steady-state achievem ent. A peculi ar at tention w as all so plaid to the thermal gradients in the *Heat Flux Probe*, to check to what extend the related measurement results would be sufficient for the further analyses.

Their results are presented below, along with their insights with respect to the test procedure and test m atrix d efinition. Note t hat no sensi tivity stu dy (r elated to grid densit y, physi cal and numerical models) was perfor med during this pre-test simulation stage, considering its actual aims; such sensitivity study will be carried on during the post-test simulation stage.

#### 5.2 Investigation of gas-liquid flow separation in ECC injection line

It is very important, for bot hith e test matrix and procedure definition, and further data interpretation, to foresee if, according to prescribed conditions, a gas-liquid flow separation may occur in the ECC injection line. Indeed, such a phenomenon occurrence has a direct impact on the outwards ECC jet form, velocity distribution and impulse, which results in a huge influence on the mixing process in the impinging jet area and downstream coldlegs tratified area (including the free surface behaviour).

The related pre-t est investigation was carried out thanks to NEPTUNE\_CFD simulations in air/water and steam/water configurations, according to a two-step procedure:

(i) firstly, a gradual uncovering of the cold leg from an initial water-filled configuration down to a 50 % water level, along with an ECC injection at a large eno ugh constant flowrate providing a single-phase flow in the injection line;

(ii) then, a continuously time-decrease of ECC flowrate down to the flowrate the reshold resulting in a clear gas-liquid flow separation along the ECC line, followed by a flowrate increase to check for any possible hysteresis. The latter increase was either a continuous one or a step-by-step one.

For both air/ water and steam /water configurations, this CFD-based investigation showed that during the ECC flowrate decrease stage (Figure 5) (i) a first gas "bubble" appears at the upper circumferential location of the ECC line orifice (onset of flow separation) and (ii) the gas phase upstream propagates along the upper section of the ECC line after a slight additional ECC flowrate decrease. The flowrate threshold providing a clear gas-liquid flow separation in the ECC line is very similar for the two fluid configurations, but it slightly depends on the initial configuration of the cold leg: if the ECC injection starts while the cold leg is already (partially) uncovered instead of being water-filled, the flowrate threshold resulting in the gas-liquid flow separation in the ECC line might be higher than previously-obtained one, depending on initial ECC flowrate.

For the subsequent ECC flowrate increase stage, the investigation demonstrated the existence of a hysteresis phenomenon (with respect to the flow separation in the cold leg), much higher for the air/water configuration than for the steam/water one. Actually with the same ECC flowrate range, water-filled ECC line was not recovered in the former configuration whereas it was in the latter one, with a higher flowrate than the afore-computed threshold; furthermore note that the hysteresis amplitude d epends on the characteristics of the flowrate increase evolution: the continuously time-increase evolution has result ed in a higher "recovering flowrate" than the step-by-step one.

These different insights resulted in recommendations for both:

- (i) the test m atrix defi nition, which took care of the anticipated ECC fl owrate th reshold values, and planned dedicated tests with respect to this ECC line flow separation concern;
- (ii) the test procedure. Tests are to be performed with an initially water-filled cold leg.

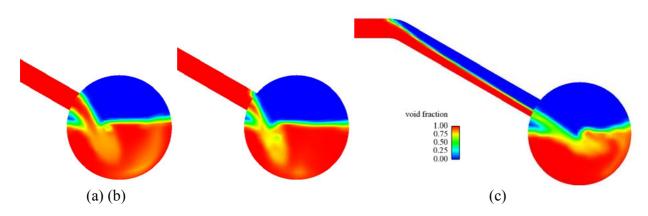


Figure 5 Flow pattern in the ECC injection line: (a) single-phase flow, (b) gas "bubble" at the ECC line orifice, and (c) gas-liquid flow separation along the ECC line

# 5.3 Check of the representation of the key physical phenomena

#### 5.3.1 Operation of the pump simulator

As p reviously i ndicated (§ 2.2), hot wat er is supplied at the top of the pump simulator to establish a counter-current flow along the cold leg upstream from the ECC injection orifice (and also to allow a faster steady state achievement), whereas water can be drained at its lowest point to avoid unphysical accumulation of hot water upstream from the ECC line.

A very first pre-test simulation of an air/water configuration indicated that the joint water supply and drainage of the pump simulator resulted in the form ation of an u ndesired circulation loop (Figure 6). The injected hot water does not penetrate much into the cold leg and rather tends to directly flow into the pump simulator to be further drained. The formation of this loop prevents from reaching the foreseen goal, and it was decided that the air/water steady-state experimental tests would be performed without any drainage of the pump simulator.

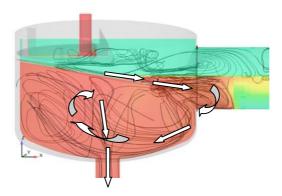


Figure 6 Flow loop in the pump simulator

# 5.3.2 Investigation of the thermal stratification in the cold leg

#### (i) Air water configuration (Figure 7)

By buoyancy and dynamic effects, ECC cold water from the injection line flows to wards the bottom of the cold leg, initially filled with hot water. After a few seconds, it reaches the cold leg wall on the opposite side of the ECC line orifice, leading to a strong mixing and cooling in the impinging jet area. The cold water flows upstream towards the pump and downstream towards the downcomer while forming a thermal stratification; therefore, a reverse flow of hot water appears in the upper part of the cold leg.

Since there is a hot water injection upstream from the impinging jet area (coming from the water feeding the pump simulator), a thermal stratification is observed in the upstream part of the cold leg. Downstream from the impinging jet area, the thermal stratification weakens with time since there is no hot sour ce to maintain the stratification, and finally, a perfect mixing is obtained. Figure 7 which represents the liquid temperature T evolution in the cold leg illustrates this final state ( $T_{max}$  and  $T_{ECC}$  are respectively the initial cold leg temperature and ECC temperature).

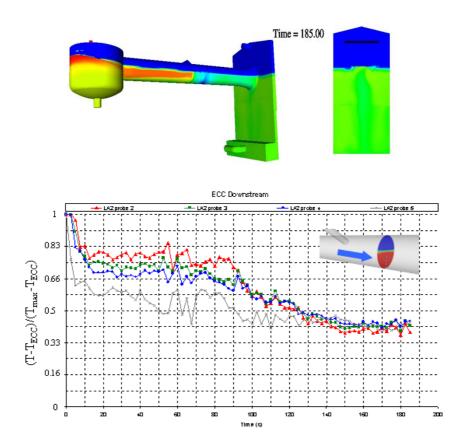


Figure 7 Air/water configuration. Stratification in cold leg

As a n important result, only the initial transient stage of a ir/water configuration tests is interesting and can provide valuable information regarding TOPFLOW-PTS program purposes; there is definitely no relevant use of the final steady-state operation.

# (ii) Steam/water configuration (Figure 8)

The same physical phenomena as those described for the air/water configuration are observed in the steam/water configuration.

But di rect contact condensation of steam along the free surface allows to maintain a thermal stratification on bo th sides of the ECC nozzle, and to eventually achieve a final steady-state stratification along the cold leg, with very valuable measurement results for the assessment and validation of the involved CFD models. Figure 8 illustrates this final state with the stratification and its thermal gradient all along the cold leg ( $T_{sat}$  is the initial temperature of water and steam in the cold leg).

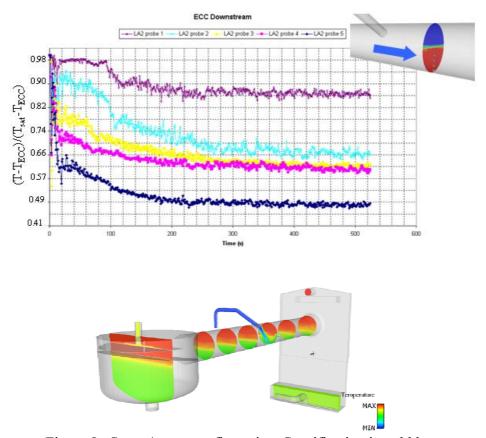


Figure 8 Steam/water configuration. Stratification in cold leg

# 5.3.3 Investigation of the temperature gradient in the Heat Flux Probe

For the afore-presented steam/water configuration simulation, the time-evolution of the wall temperature distribution in the heat flux probe is plotted at the location of the immersed thermocouple (Figure 9).

It shows that the related thermocouple measurements within the as-designed HFP can result in significant temperature differences along a transient PTS-type test, and will be very useful to a assessment of the whole modeling involved in the coupled "CFD-heat conduction" simulation of a PTS scenario.

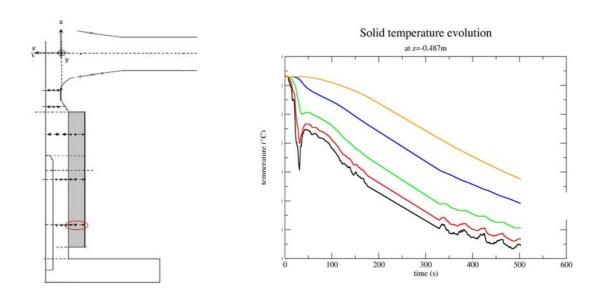


Figure 9 Temperature evolution in the Heat Flux Probe for one elevation and five depths

#### 6 Conclusion

TOPFLOW-PTS Experimental Program is an integral-type program related to the CFD modeling of a PTS two-phase flow configuration. The purpose is to provide a well documented database to perform the validation of CFD models in two-phase flow configurations, and to improve the knowledge and the understanding of the involved key physical phenomena. In this frame, pretest simulations were carried out with NEPTUNE\_CFD code to help in the definition of the test matrix, and possibly of the test procedure, making sure the different key physical phenomena of interest are actually present and can be "caught" by the implemented instrumentation.

These pre-test simulations have pointed out the following main insights:

- (i) a gas-liquid flow separation occurs in the ECC injection line when the flowrate becomes lower than a threshold value. It is an actual concern to be accounted for since it strongly modifies the mixing phenomena in the impinging jet area and do wnstream stratified cold leg area;
- (ii) no relevant steady-state can be ach ieved in an air/water configuration, op posite to the steam/water configuration for which a st eady-state stratification can be m aintained all along the cold leg thanks to the direct contact condensation of steam;
- (iii) for relevant PTS transient tests, the temperature measurements within the implemented *Heat Flux Probe* should allow a assessment of the whole coupled "CFD-Heat conduction" simulations.

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